# THE EFFECT OF FREEZING AND THAWING ON THE DEWATERING OF OIL SANDS SLUDGES<sup>1</sup>

by

Richard L. Johnson<sup>2</sup>, Peter Bork<sup>3</sup>, Paul Layte<sup>2</sup>

Oil sands processing operations in Abstract. northeastern Alberta generate 25 X 106 mэ of water-fines mixtures (sludge) per year. The fines settle in several weeks but will not consolidate to more than 35% solids, even over centuries. Freezing and thawing the oil sands sludge led to rapid dewatering. One cycle of freezing and thawing caused 15, 25, 35, and 45% solids sludge to reach 35, 39, 48, and 51% solids content. respectively. Subsequent freeze-thaw cycles, up to a total of three, caused less rapid increases in solids content. The maximum concentration of solids by freezing and thawing, even after repeated cycles, was 60%. The amount of dewatering due to freeze-thaw can be confidently predicted by knowing only the initial solids content. The freezing time for each sludge concentration was monitored to compute proportionality coefficients required to predict freezing depths under field conditions.

Additional Key Words: slurries, tailings, Neuman-Stefan proportionality coefficient, solids concentration.

- Paper presented at the 1989 International Symposium on Reclamation, A Global Perspective, sponsored by the Canadian Land Reclamation Association and the American Society for Surface Mining and Reclamation, Calgary, Alberta, August 27-31, 1989.
- <sup>2</sup> Richard, L. Johnson and Paul Layte are Branch Heads of Soils and Engineering and Instrumentation, respectively, Alberta Environmental Centre, Vegreville, Alberta, Canada TOB 4LO.
- <sup>3</sup> Peter 8ork is Engineer, Terro Con Geotechnic Ltd., Suite 201, Nisku Centre, 8ox 548, NISKU, AB TOC 2GO Proceedings America Society of Mining and Reclamation, 1989 pp 687-694 DOI: 10.21000/JASMR89020687

https://doi.org/10.21000/JASMR89010687

# Introduction

The enormous volumes of oil sands tailings generated by two extraction and upgrading plants located near Ft. McMurray, Alberta. pose economical and ecological problems in land reclamation. Approximately 170,000 barrels of synthetic oil per day is produced from 400,000 tonnes of oil sands; the tailings stream amounts to 180 million metric tonnes per year and currently occupies 25 km<sup>2</sup>.

Sludge, a mixture of fines diameter), (<22 microns water. and residual bitumen, is the most difficult component in the tailings stream to handle for reclamation. The sand portion of the tailings stream segregates from the slurry upon deposition at the edge of the tailings pond and is used to build the pond dikes. Thin sludge, at approximately 5% solids content, flows into the pond and settles to a solids content of 20 to 30% within two years. The sludge 250 million volume now exceeds and is mз increasing at the rate of 20 million mэ per Consolidation to 80% annum. solids, representing a firm. stable surface, is expected to take tens of thousands of years if left to mature under natural conditions (Scott et al. 1985).

The most recent research at the Alberta Environmental Centre explores the possibility of using vegetation to dewater relatively thin layers of sludge (<3 m) through evapotranspiration (Johnson et al. 1989). Two species of hydrophilic plants, reed canary

grass (Phalaris arundinaceae) and dock (Rumex occidentalis) have proven successful sma]] on а scale. However. to establish plants quickly and achieve complete dewatering in one summer, a bed of at least 50% solids sludge is needed. Among the alternatives to increase the solids content of oil sands sludge 30% from to 50%. dewatering freezing by and thawing appears to be most efficient and economical.

Freeze-thaw originated as a dewatering technique in temperate climates where biological sludges were concentrated from 3-5% solids to >30% solids (Downes, 1939. Clements et al. 1950, Bishop and Fulton, 1968, Logsdon and Edgerly 1971, Rush and Stickney 1979). Preliminary tests on the effect of freeze-thaw oil on sands sludge caused a large increase in percent solids (Johnson et al. Since Ft. McMurray has 1989). long, cold winters, freezing and thawing could be a low cost. efficient means of dewatering oil sands sludge on a field scale.

To develop a rational engineering procedure for freeze-thaw dewatering, the environmental factors that control frost be quantitied penetration must (Martel 1989). The Neuman-Stefan formula for predicting the formation of ice on lakes should apply liquid sludges also to (Reed et al. 1986). This formula requires information on the freezing index of location а (Rush and Stickney 1979) and a coefficient for proportionality the material being frozen or thawed, which depends upon its

thermal conductivity and latent heat. One objective of the research described here is to calculate a Neuman-Stefan coefficient for oil sands sludge.

### <u>Materials</u> and Methods

freeze-thaw experiment This on oil sands sludge was carried out under pilot plant scale conditions: experimental units were barrels with a capacity volume of approximately 60 L; sludge was diluted with water to four solids contents using a rotor attached to an electric drill; the sludge was frozen by placing the barrels inside a walk-in freezer and thawed by removing them from the freezer and letting them stand in a open work space.

## Experimental Units.

The experimental units were constructed by placing an interior metal drum into an exterior polyethylene drum (Figure 1). To simulate natural freezing conditions, where the freezing front progresses from the surface downward, insulation was inserted between the two containers and at the bottom of the inside barrel. A total of 12 experimental units were constructed to allow three replicates of four sludge dilutions.

## <u>Sludge Dilution Mixes</u>

Four sludge dilutions were chosen to represent a wide range of solids contents in the oil sands tailings ponds: 15, 25, 35, and 45% (solids, dry weight basis). These were prepared by

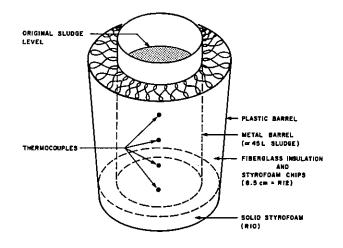


FIGURE I. EXPERIMENTAL UNIT FOR FREEZING AND THAWING OLISAND SLUDGE PLACED INSIDE AN INSULATED BARREL

sequentially diluting a batch of high solids content sludge with reverse-osmosis, deionized water. After completing each dilution, three experimental units were filled to a depth of 46 cm providing an initial volume of 45 L. Sludge sampling inside the experimental units was conducted prior to initial freezing and after every freeze-thaw cycle. All replicates were sampled at three depths: one-sixth, one-half and five-sixths of the total sludge depth. The sample sites inside the experimental unit were selected randomly, using a random number table where each number corresponded to a grid intersection placed over the sludge surface. The percent solids of the samples were determined by mass measurements before and after oven-drying (105°C for 24 h).

### Freezing and Thawing

The twelve units were placed in a completely random pattern inside the freezer. Unit location

689

randomized each time the was freezing cycle was repeated. The freezer temperature was kept at -24°C throughout the experiment. One replicate of each sludge dilution was fitted with four type thermocouples connected to a T Campbell Scientific CR 10 micrologger (Figure 1). Temperatures were recorded at four depths within each sludge dilution mix. When each thermocouple within the sludge registered frozen а maximum temperature of -20°C, the freezing period was considered complete. All units were removed from the freezer at the same time for the thaw stage.

Two days into the thaw period the units were covered with lids prevent moisture loss by to The thaw period was evaporation. considered complete once a]] units registered а minimum temperature of 20°C. The surface bitumen was skimmed off, and the thaw water was removed and volumetrically. measured The experimental units were then sampled for solids contents in the manner described above.

The freeze-thaw process was repeated three times.

# Freezing Coefficient Determination

The Neuman-Stefan formula allows for the calculation of total freezing depth (Reed et al. 1986):

$$x = m (\Delta T \cdot t) \frac{1}{2}$$
 (1)

where:

x = depth of freezing [cm], m = proportionality coefficient depending on the thermal conductivity, density, and latent heat of the material being frozen [cm/(°C.day)1/2] freezing index [°C.day].

- ΔT.t = freezing index [°C.day], ΔT = difference between the freezing temperature anda verage daily ambient temperature [°C],
  - t = time period of concern
    [days].

By rearranging the formula the proportionality coefficient for oil sands sludge can be estimated:

$$m = \frac{X}{(\Delta T \cdot t)^{1/2}}$$
(2)

The fourth thermocouple, placed at approximately 8 cm above the bottom of the sludge, was used as the freezing depth to calculate the proportionality coefficient from equation 2. Only data from the first freeze-thaw cycle was used in this calculation.

## Results

The sludge concentrations before and after each freeze-thaw in Table 1. cycle are given Individual values represent the average of samples taken at three depths within three replicates of each mix. (The exceptions to this are one replicate each from mixes 1 and 2, representing 45 and 37% solids, respectively. In both cases the metal drums failed due to pressures exerted during the freezing cycle).

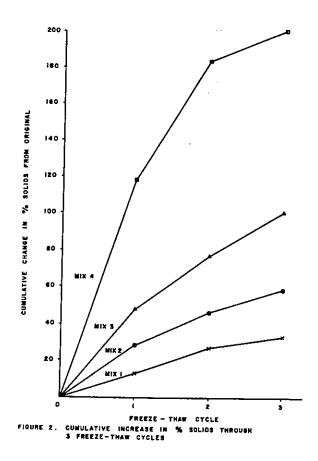
There were some small differences between the intended and actual solids contents, but the largest variance was only 2.4% (mix 2 was intended to be Table 1. Average percent solids before and after freeze-thaw cycles.

Mix	Original	Solid	s After	Freeze-	
#	Solids	Thaw Cycle			
	Content	1	2	3	
	(%)		(%)		
1	45.4	51.3	57.8	60.4	
2	37.4	47.9	55.1	59.6	
3	26.2	38.7	46.4	52.6	
4	16.3	35.4	46.2	49.5	

35% and, in fact, reached 37.4%). Overall, the desired range of solids content was achieved.

While each freeze-thaw cycle resulted in a progressive dewatering of each mix, it is apparent that the first cycle was more effective than the second which. in turn, was more effective than the third (Figure And even more noticeable is 2). the effect of initial solids content the amount on of Mix 1, starting at dewatering. solids, had a cumulative 46% increase of only 35% over three freeze-thaw cycles; mix 4, on the other hand, starting at 16% solids finished after three cycles at 49.5% solids, a 200% increase! cumulative The two intermediate dilutions also had intermediate cumulative increases in solids content (Figure 2), indicating a correspondence between initial and final solids content.

The relationship between initial solids content of oil sands sludges and the degree of dewatering through freeze-thaw



cycles is · exponential (Figure Low initial solids content 3). results in a large amount of dewatering. As the solids content increases the rate of dewatering drops quickly. The exponential decrease in rate of dewatering is independent of freeze-thaw cycle, which acts determinant only as а of "initial" solids content. The prediction of final solids content of oil sands sludge undergoing freeze-thaw can be confidently made without considering the previous freeze-thaw history of the sample:

$$Y = 365.3 (0.93) \times (3)$$

where:

Y = final solids content [%] x = initial solids content [%]

The coefficient of determination  $(r^2)$  is high – .95. Only 5% of the variation in final solids content is <u>not</u> accounted for by the initial solids content.

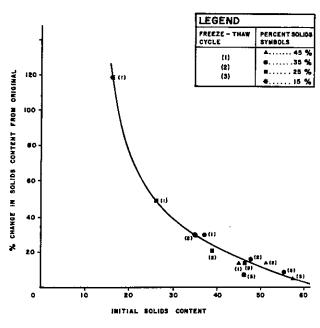


FIGURE 3. CHANGE IN FINAL SOLIDS CONTENT IN RELATION TO INITIAL SOLIDS CONTENT AND FREEZE - THAW CTCLE

The relationship between the solids content of the initial sludge and the calculated Neuman-Stefan proportionality coefficients are given in Table 2. For mixes with solids contents less linear than 45%. there is a relationship between the Neuman-Stefan proportionality constant (m) and the initial solids content such that:

Table 2. Neuman-Stefan proportionality coefficients for oils and sludge mixes.

Original solids content (%)	<u>Freezin</u> hours	<u>g Time</u> <u>days</u>	Proport- tionality constant (m)
45.4	125	5.2	3.41
37.4	177	7.4	2.86
26.2	195	8.1	2.73
16.3	217	9.0	2.59

### $m = 0.0128 \times + 0.998$ (4)

where:

x = initial solids content [%]

The coefficient of determination is 0.996. For the mix with an initial solids content of 46%, the proportionality coefficient is much higher than that which might be predicted by equation 4.

# Discussion

The experimental results confirm previous findings at the Alberta Environmental Centre that the freeze-thaw process increases the solids content of oil sands sludge (Johnson et al. 1989). originating The mineral fines from bitumen extraction processes have less than two percent organic contents (Scott et al. 1985). but like act sewage subjected sludges when to freeze-thaw conditions (Rush and 1979). The Stickney sludge mixtures with the lowest solids content, mineral or organic. dewater to the greatest extent. There is an exponential decrease in the amount of water released

as pre-freezing solids contents increase. Multiple freeze-thaw cycles cause progressive loss of water, but the same exponential relationship between original solids contents and amount of water loss applies. That is, the second and third and more freeze-thaw cycles are acting on mixtures with higher and higher solids contents and, therefore, there is an exponential decrease in the amount of water lost with each cycle.

The oil sands sludges tested in this experiment reach а maximum of approximately 60% solids contents, if subjected to enough freeze-thaw cycles (Table 2, Figure 3). On an operational basis the sludge accumulating at the bottom of the tailings pond on the Syncrude Canada Limited lease reaches a maximum of 35% solids in two to five years; according to equation 3 and Table 2, one winter of freezing and thawing will yield sludge at 45% solids content. This has been corroborated in a recent field experiment conducted in Ft. McMurray (Johnson et al. 1989).

One proposed reclamation scheme for oil sands sludge involves the use of plants to dewater sludge through evapo-transpiration. To successfully establish plants а relatively bed is firm seed needed, corresponding approximately to 50% solids content. One winter will produce the desired seed bed conditions, a sludge surface at 45-50% solids, depending on the depth of sludge frozen, the type drainage employed, and the of amount of moisture lost through

evaporation prior to the establishment of the plants.

The proportionality coefficients for the Neuman-Stefan formula have a linear relationship to original solids contents. the This formula is used to estimate the depth of freezing achievable in a selected time period (Reed et al. 1986) and can now be used confidently to design facilities and treatment programs for oil sands sludges, where the thickness of individual layers and the time periods for freezing are critical constraints. Work is currently underway at the Alberta Environmental Centre investigating a dynamic (multiple layers) freeze-thaw process for oil sands sludges.

# <u>Literature Cited</u>

- Bishop, S.L. and G.P. Fulton. 1968. Lagooning and freezing for disposal of water plant sludge. Public Works 99:94-96.
- Clements, G.S., R.J. Stephenson, and C.J. Regan. 1950. Journal of the Institute of Sewage Purification Part 4, pp. 318-339.
- Downs, R. 1939. Sludge dewatering by freezing. Water Works and Sewage (1939) p. 282.
- Johnson, R.L., E.A.D. Allen, L. Koverny, W. James and A. Boni. 1989. Biological dewatering of Athabaska oil sands sludge. RRTAC Report (in preparation). Edmonton, Alberta.

- Logsdon, G.S. and E. Edgerley Jr. 1971. Sludge dewatering by freezing. American Water Works Association Journal 63:734-740.
- Martel, C.J. 1989. Dewaterability of freeze-thaw conditioned sludges. Journal of the Water Pollution Control Federation 61:237-241.
- Reed, S., J. Bouzoun, and W. Medding. 1986. A rational method for sludge dewatering via freezing. Journal of the Water Pollution Control Federation. 58:911-916.
- Rush, R.J. and A.R. Stickney. 1979. Natural freeze-thaw sewage sludge conditions and dewatering. Report No. EPS 4-WP-79-1. 40 pp. Environment Canada, Waste Water Technology Centre, Burlington, Ontario.
- Scott, J.D., M.B. Dusseault and W.D. Carrier. 1985. Behavior of the clay/bitumen/water sludge system from oil sands extraction plants. Applied Clay Science 1:207-21B.

https://doi.org/10.1016/0169-1317(85)90574-5